

SPASSKAYA, R.I.; KAZARNOVSKIY, S.N.

Continuous method of producing guanidine from urea. Khim.prom.
no.7:488-491 Jl '63. (MIRA 16:11)

ANTIPINA, I. V.; KAZARNOVSKIY, S. N.; Prinimala učastiy: LEBEDEVA
V. V.

Oxidation of cyclohexylamine by hydrogen peroxide to cyclohexanone
oxime. Khim prom no. 3:165-170 Mr '64. (MJRA 17:5)

MALKINA, N.I.; KAZARNOVSKIY, S.N.

Synthesis of cyanuric acid from urea. Zhur.prikl.khim. 37
no. 5:1158-1160 My '64. (MIRA 17:7)

1. Gor'kovskiy politekhnicheskiy institut imeni A.A.Zhdanova.

L 10407-66

ACC NR:

EWT(m)/EMP(w)/EMP(j)/T/EMP(t)/EMP(b)

Monograph

JD/WB/DJ/ME/RM

AM5022503

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Kolotukhin, Ivan Nikiforovich; Kuznetsov, Vasiliy Georgiyevich; Kazarnovskiy,
Semen Naumovich; Tsaregradskiy, Vladimir Alekseyevich

Lubricating and protective materials (Smazochnyye i zashchitnyye materialy) 17/
3d ed., rev. and enl. Moscow, Izd-vo "Transport," 1965. 171 p. illus.,
biblio., 8000 copies printed.

TOPIC TAGS: lubricant, lubricant component, lubricant property, lubricating oil,
grease, lubrication, paint, lacquer, detergent, railway rolling stock,
protective coating, corrosion protection

PURPOSE AND COVERAGE: This monograph presents the basic properties, test and
preparative methods, and also applications for lubricant and protective
paints and lacquers required in the railroad industry. Compared with the
second edition, this edition provides additional information on synthetic
oils/greases, new synthetic polymeric paints and lacquers, and also detergents
and polishing compositions. The monograph was approved by the State Admin-
istration for Educational Institutions of the Ministry of Transport as a
textbook for rail transport technical schools and can be used by a wide range
of workers who are connected with painting and lubrication of rolling stock.

Card 1/3

UDC: 625.23/.24002.4:[621.892+66]

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APPROVED FOR RELEASE: 06/13/2000

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KOLOTUKHIN, Ivan Nikiforovich; KUZNETSOV, Vasiliy Georgiyevich;
KAZARNOVSKIY, Semen Naumovich; TSAREGRADSKIY, Vladimir
Alekseyevich; SALTANSEV, Yu.S., red.

[Lubricating and protective materials] Smazochnye i zashchit-
nye materialy. Izd.3., perer. i dop. [By] I.N.Kolotukhin,
i dr. Moskva, Transport, 1965. 171 p. (MIRA 18:4)

KAZARNOVSKIY, V.

[Analysis of the financial administration of industrial enterprises]
Analiz khokhiaistvennoi deiatel'nosti promyshlennogo predpriatiia.
Moskva, Gosfinisdat, 1954. 133 p.
(Industrial management) (MLRA 7:12)

Translation from: Referativnyy zhurnal, Geologiya, 1957, Nr 4,
p 184 (USSR) 15-57-4-5393

AUTHORS: Borisova, E. A., Kazarnovskiy, V. D.

TITLE: Laboratory Investigations on the Treatment of Saline
Soil by Liquid Bitumen With Preliminary Flushing by
Water (Laboratornyye issledovaniya po obrabotke zasolen-
nykh gruntov zhidkim bitumom s predvaritel'noy promyvkoj

PERIODICAL: Tr. Mosk. avtomob.-dor. in-ta, 1956, Nr 18, pp 241-248.

ABSTRACT: The material used was chloride-sulfate saline soil cut
from a section of rock in the Andizhanskaya Oblast',
Uz SSR. The data of the investigations are given. It
was discovered that when the chloride and sulfate
content of soil exceeds one percent, the soil is
unsuitable for treatment with organic binding material
in highway construction and demands preliminary flushing
by water. The authors outline the relationship between
number of flushings of the soil by water and the quantity

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Laboratory Investigations on the Treatment of Saline (Cont.) 15-57-4-5393

of indroducible bitumen. They show the possibility of lowering the
quantity of binding substance by increasing the number of flushings,
and, on the other hand, lowering the number of flushings by somewhat
increasing the expenditure of binding substance, depending on the
economy of the construction. It is noted that flushing of the soil
has not yet been applied in highway-construction practice. However,
flushing the soil before treating with liquid bitumen may prove to be
much more profitable than replacing the saline soil. The results
obtained from testing samples by composite flushing of soil and use
of liquid bitumen (bulk weight, water saturation, swelling, dura-
bility of dry and capillary-moistened samples) are in agreement,
according to the degree of fitness of saline soils, with the classi-
fication of the "Technical rules on the construction of a roadbed
and highway base in the desicated zone on saline soils." Flushing
of the soil (2 to 3 times) is proposed for the roadbed immediately
next to the highway. For flooding sections of the earthen roadbed,
it is necessary to construct retaining borders of planking or of low
soil ridges.

Card 2/2

Ye. G. B.

KAZARNOVSKIY, V.D., inzh.; KAZARNOVSKAYA, E.A., inzh.

Washing salty soils for road construction. Trudy MADI no.22:
170-175 '58.
(Soil physics) (Road construction) (MIRA 12:4)

KAZARNOVSKIY, Vladimir Davydovich; GANYUSHIN, A.I., red.; MAL'KOVA,
N.V., tekhn. red.

[Calculation of the shear strength of soil in the designing of
a road] Uchet soprotivliaemosti grantov svigigu pri proektirova-
nii dorozhnoi konstruktsii. Moskva, Avtotransizdat, 1962. 34 p.

(Soil mechanics)

(Roads—Designing)

(MIRA 15:5)

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KAZARNOVSKIY, V.D., inzh.

Degree of soil stabilization and the shear resistance of ground,
Avt.dor. 24 no.12:15-17 D '61. (MIRA 14:12)
(Soil stabilization)

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MASLOV, N.N., prof., doktor tekhn.nauk, zasluzhennyy deyatel' nauki i
tekhniki FSSR; KAZARNOVSKIY, V.D., inzh.

Using the density-humidity method in determining soil
resistance. Avt.dor. 25 no.12:19-21 D '62. (MIRA 16:2)
(Soil mechanics)

FUZAKOV, N.A., doktor tekhn. nauk; KHARKHUTA, N.Y., doktor tekhn. nauk; MOTYLEV, Yu.L., kand. tekhn. nauk; VEYLENAN, M.I., kand. tekhn. nauk; MITASOV, I.V., inzh.; LEVITSKIY, Ye.F., inzh.; RUMANOV, A.Z., inzh.; Prinimali uchastiye: LAZAROVSKIY, V.D., kand. tekhn. nauk; DENISOV, Ye.M., inzh.; TOPOL'NITSKAYA, L.F., red..

[Instruction for building earth automobile roadbeds] Instruktsiya po sooruzheniiu zemlianogo polotna avtomobil'nykh dorog (VSM 97-63). Moskva, Transport, 1964. 238 p.

(MIRA 17:11)

l. Russia (1923- U.S.S.R.) Gosudarstvennyy proizvodstvennyy komitet po transportnomu stroitel'stvu.

KAZARNOVSKIY, Ya. S.

"The Explosive Conversion of Methane, Part 1", Khimicheskaya
Pererabotka Neftyanikh Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 133-141

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KAZARNOVSKIY, Ya. S.

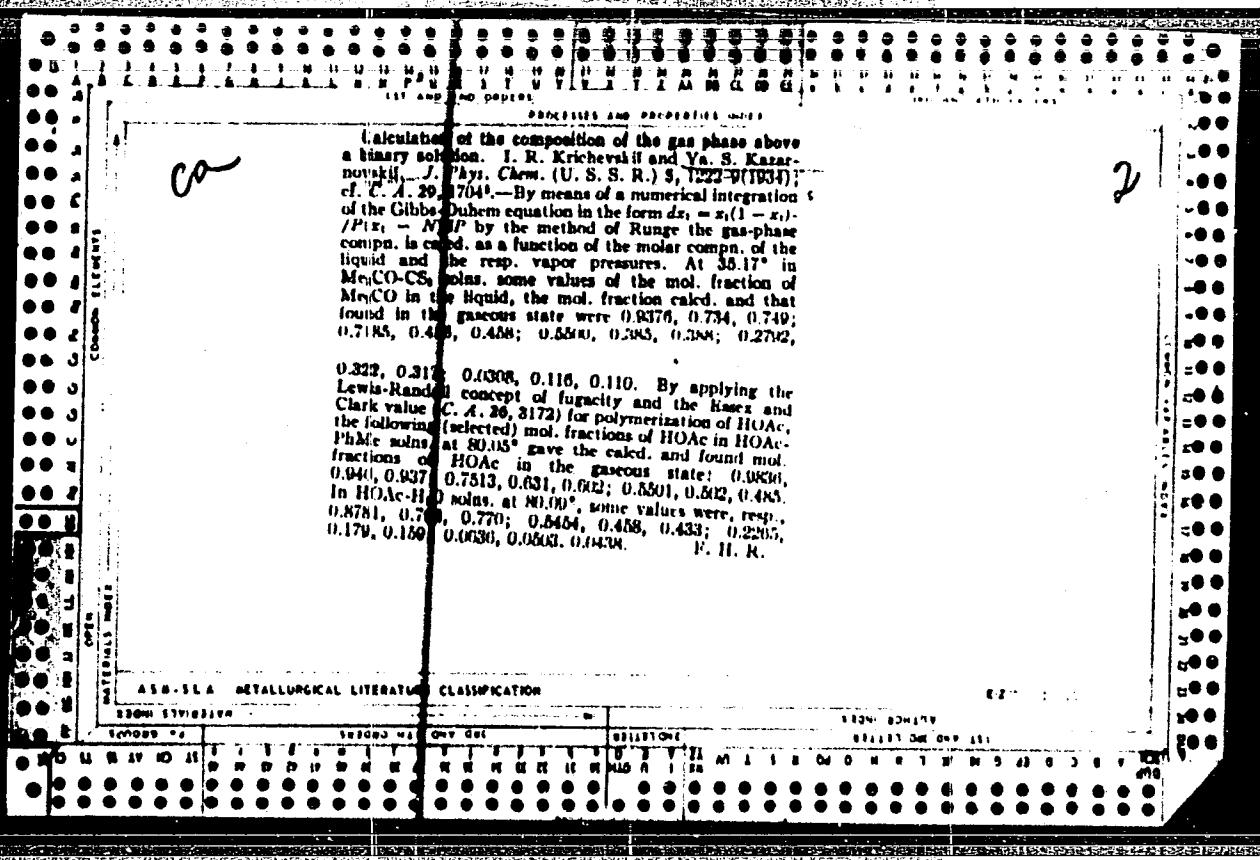
"The Explosive Conversion of Methane, part 2", Khimicheskaya
Pererabotka Neftyanых Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 142-152

S4M1 16/24

RAZARNOVSKIY, Ya. S.

"The Explosive Conversion of Methane; Part 2," Khimicheskaya
Pererabotka Neftyanikh Uglevodorodov (Chemical Conversion of Petroleum
Hydrocarbons), Academy of Sciences USSR, Moscow, 1956, pp 153-166

SUM 11/39



BC

C-1

Explosive combustion of methane. N. Kossov, J. Kazarinov, and I. Karshmanov (Acta Physico-Chim. URSS, Proc., 3, 807-816).—The yield of CO₂, H₂O, SO, and H₂ per cu.m. of CH₄ consumed in an explosive mixture of CH₄ and O₂ is independent of pressure up to 370 atm. and is unaffected by the nature of the wall or the diameter of the vessel, although the amount of CH₄ oxidized is less in narrow vessels. The influence of additions of N₂, CO, CO₂, and H₂ is in agreement with thermodynamic requirements. The explosion temp. calc. from the water-gas equilibrium data agrees closely with that calc. from exp. heat data, and it is inferred that equilibrium is attained in the explosion. If H₂O is present initially CH₄O and EtOH are formed and equilibrium is not attained. The reaction forms a suitable source of H₂ for the NH₃ synthesis.

R. S.

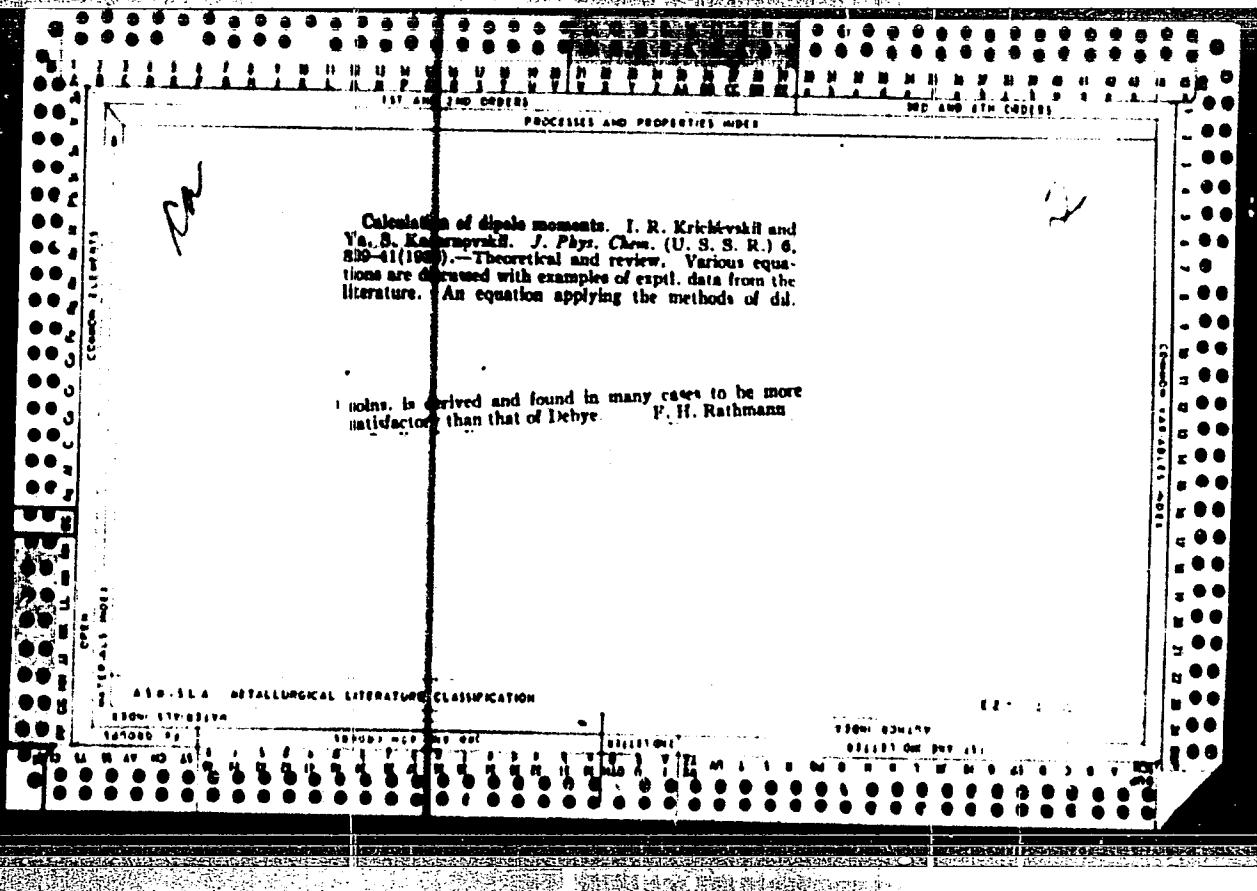
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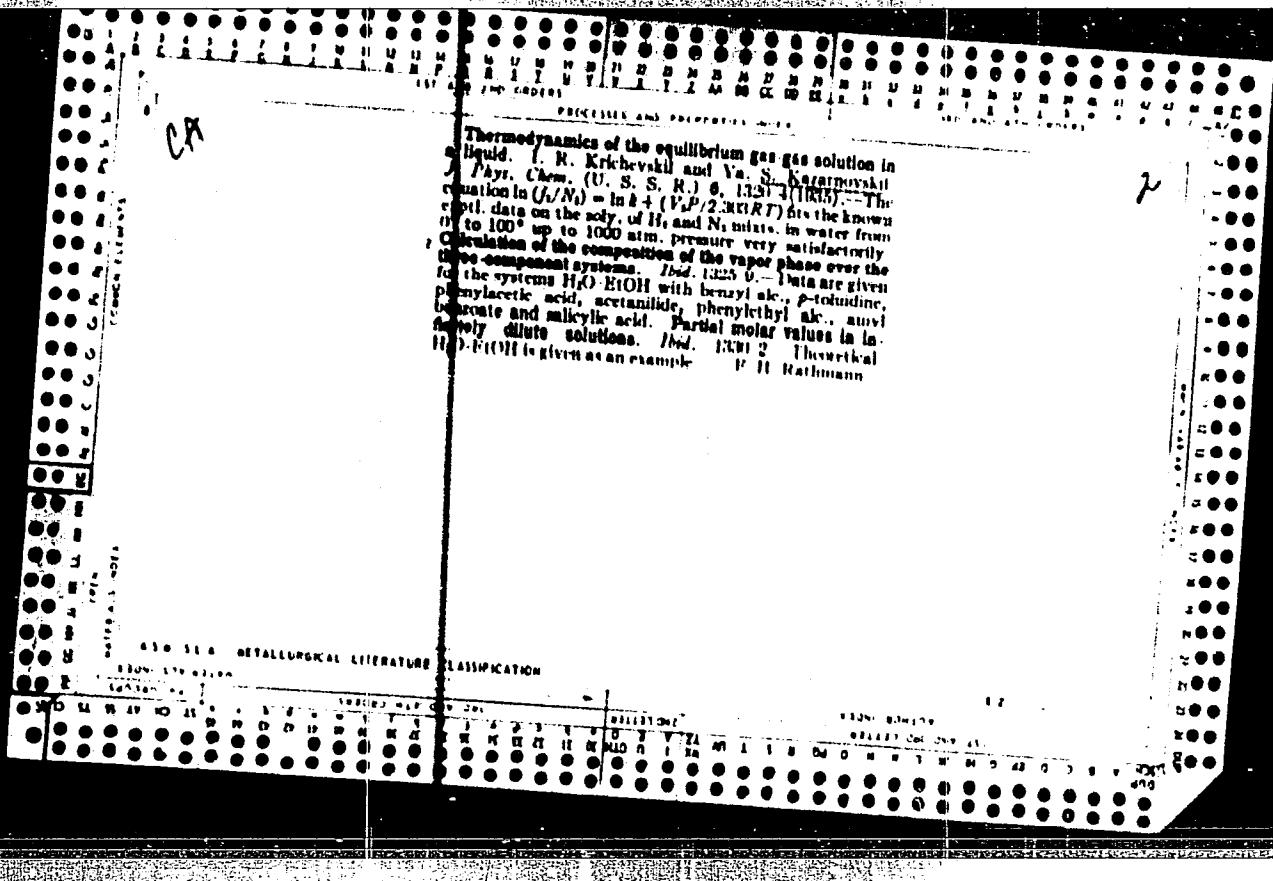
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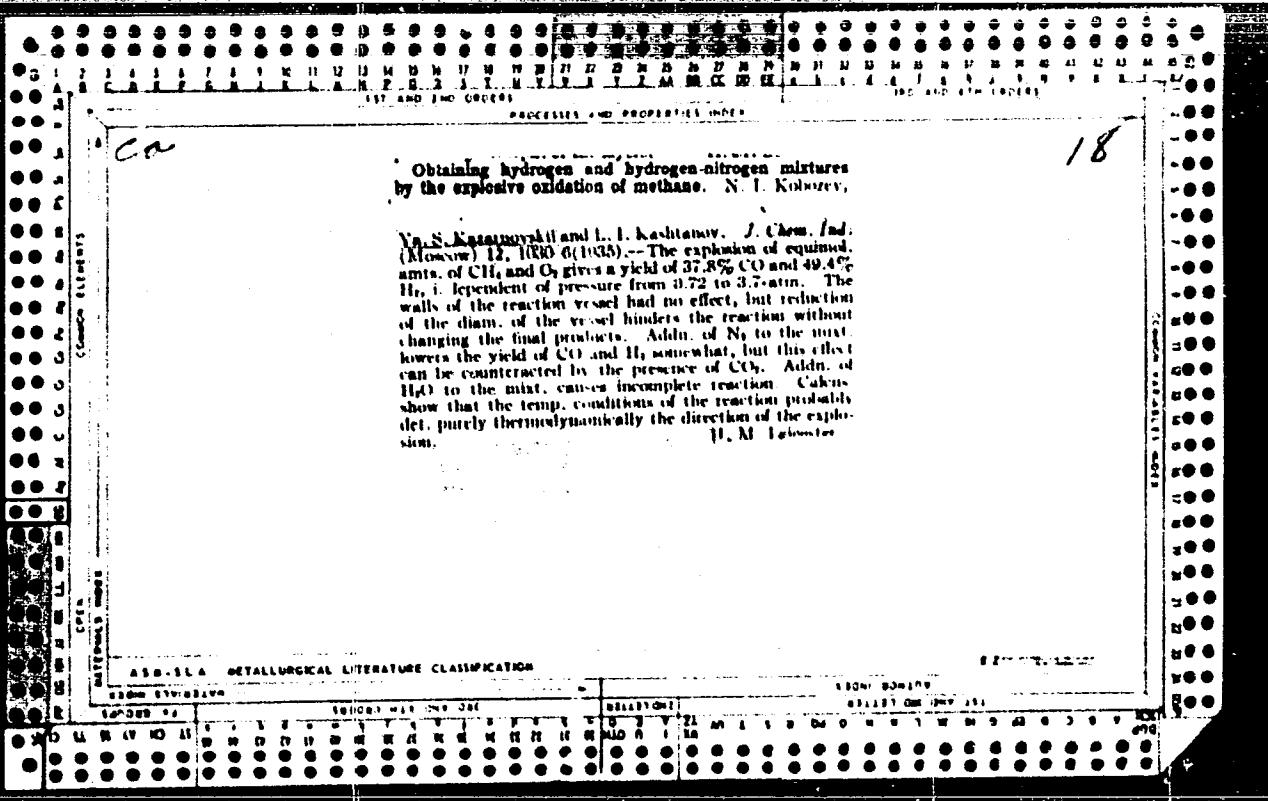
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180000-85 | 180000-86 | 180000-87 | 180000-88 | 180000-89 | 180000-90 | 180000-91 | 180000-92 | 180000-93 | 180000-94 | 180000-95 | 180000-96 | 180000-97 | 180000-98 | 180000-99 | 180000-100 | 180000-101 | 180000-102 | 180000-103 | 180000-104 | 180000-105 | 180000-106 | 180000-107 | 180000-108 | 180000-109 | 180000-110 | 180000-111 | 180000-112 | 180000-113 | 180000-114 | 180000-115 | 180000-116 | 180000-117 | 180000-118 | 180000-119 | 180000-120 | 180000-121 | 180000-122 | 180000-123 | 180000-124 | 180000-125 | 180000-126 | 180000-127 | 180000-128 | 180000-129 | 180000-130 | 180000-131 | 180000-132 | 180000-133 | 180000-134 | 180000-135 | 180000-136 | 180000-137 | 180000-138 | 180000-139 | 180000-140 | 180000-141 | 180000-142 | 180000-143 | 180000-144 | 180000-145 | 180000-146 | 180000-147 | 180000-148 | 180000-149 | 180000-150 | 180000-151 | 180000-152 | 180000-153 | 180000-154 | 180000-155 | 180000-156 | 180000-157 | 180000-158 | 180000-159 | 180000-160 | 180000-161 | 180000-162 | 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180000-702 | 180000-703 | 180000-704 | 180000-705 | 180000-706 | 180000-707 | 180000-708 | 180000-709 | 180000-710 | 180000-711 | 180000-712 | 180000-713 | 180000-714 | 180000-715 | 180000-716 | 180000-717 | 180000-718 |
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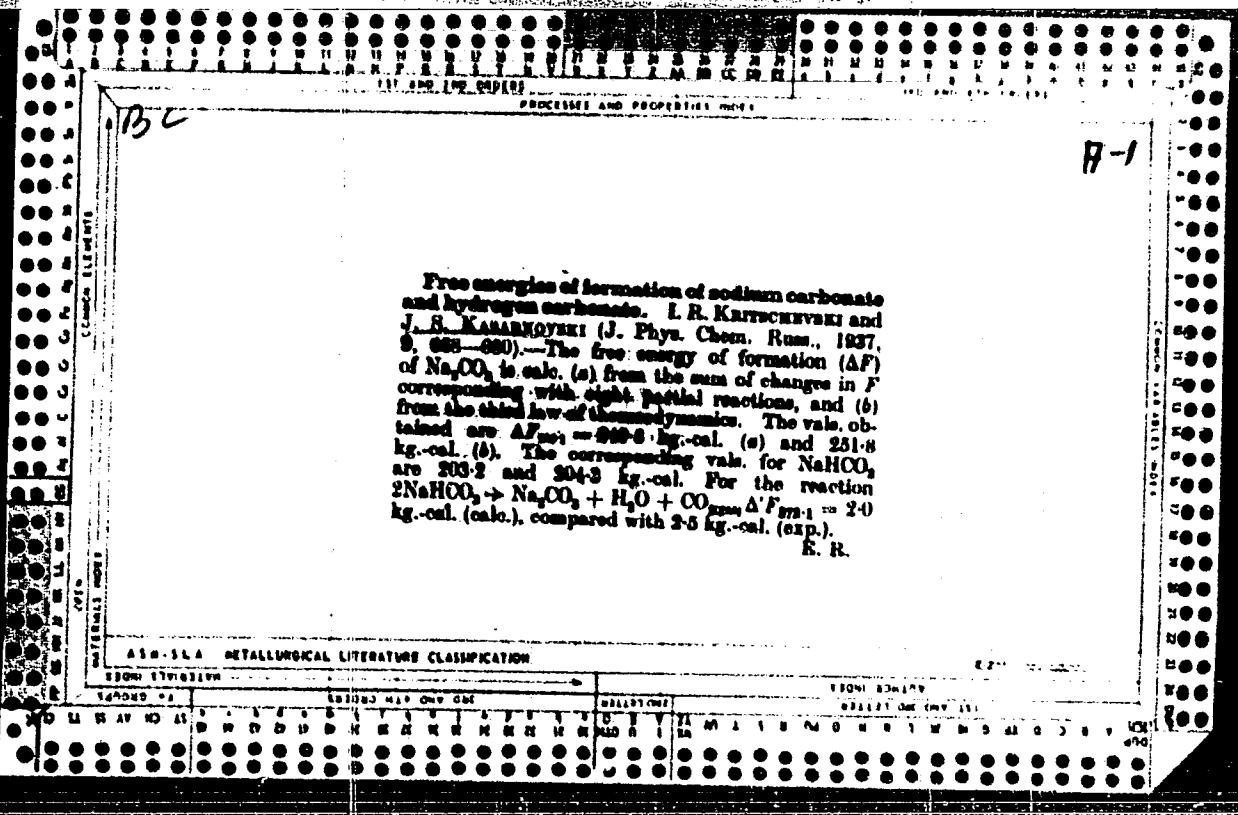


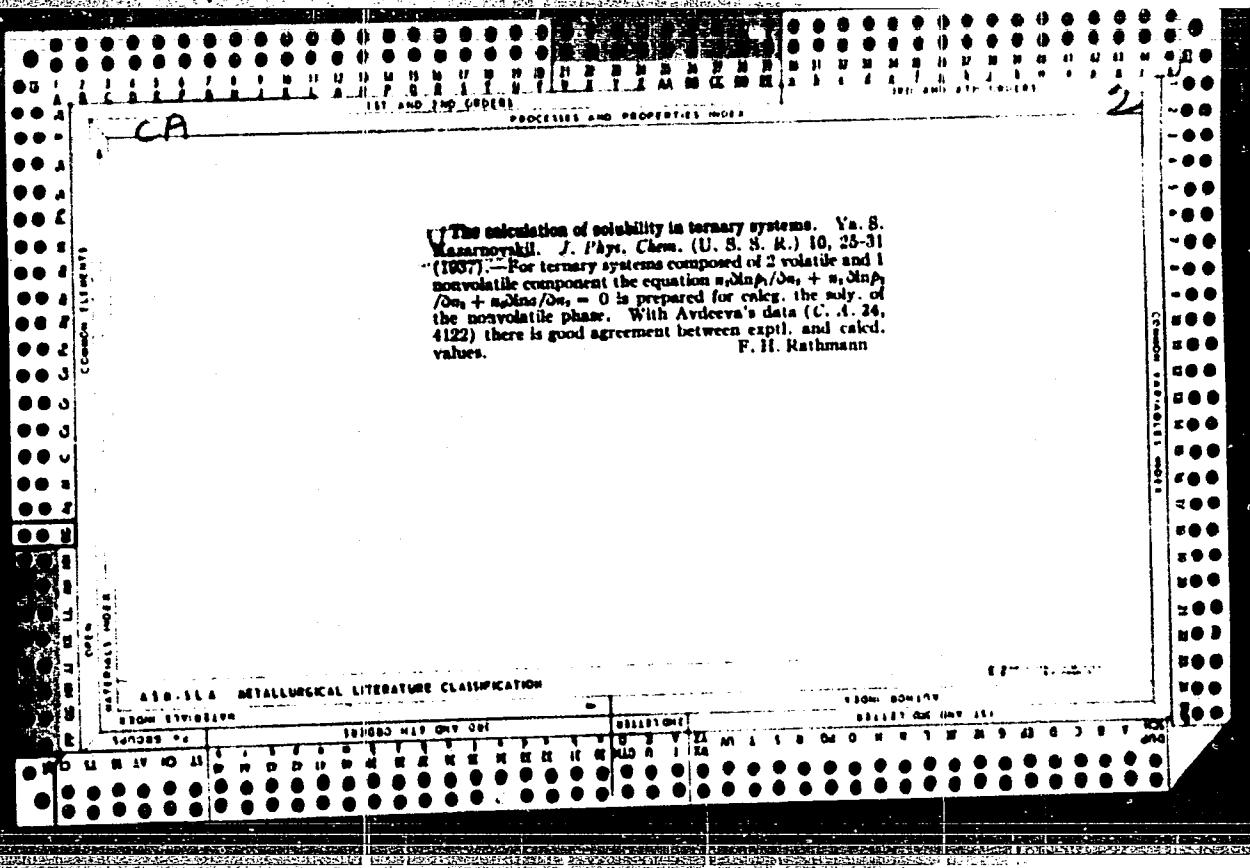


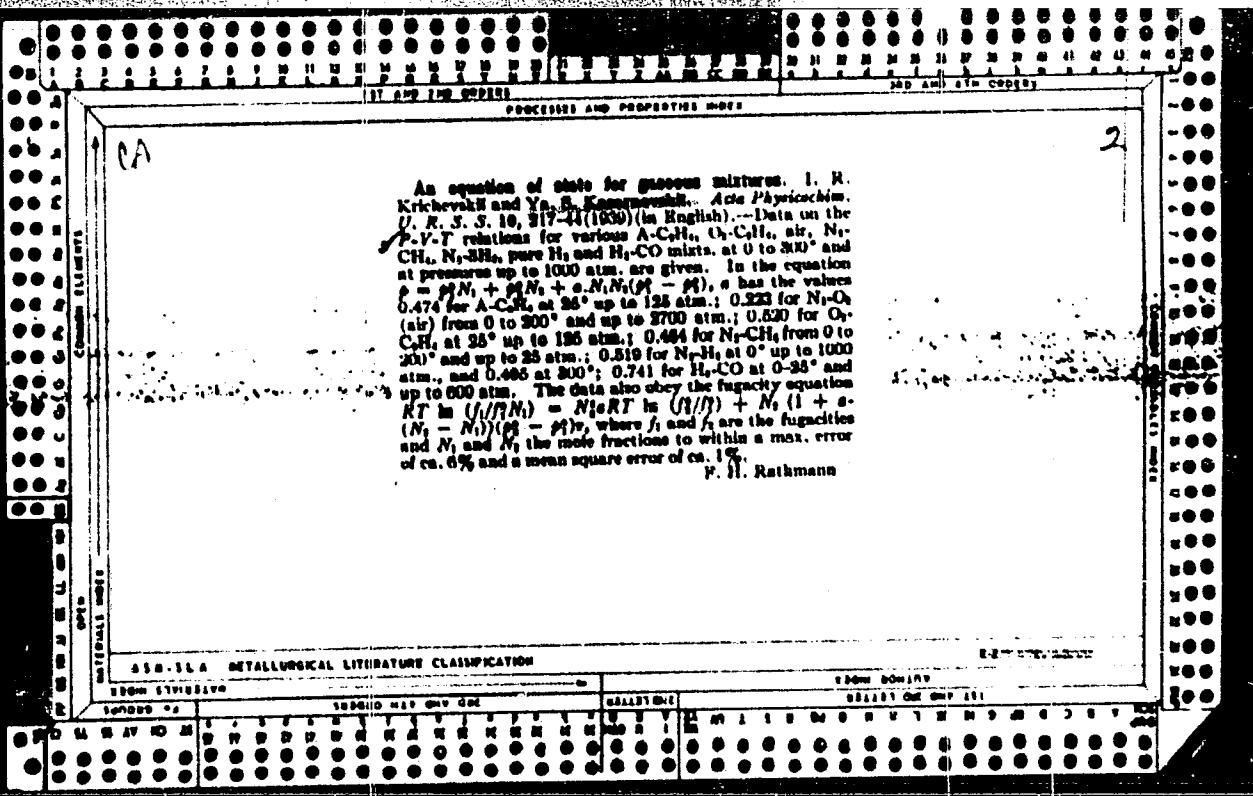
Solubility in ternary systems. J. S. KAZARNOVSKI (J. Phys. Chem. Russ., 1937, 9, 28-31).—The solubility of a non-volatile component in a mixture of two volatile solvents has been calc. for the system $\text{NaCl} + \text{H}_2\text{O} + \text{NH}_3$. E. R.

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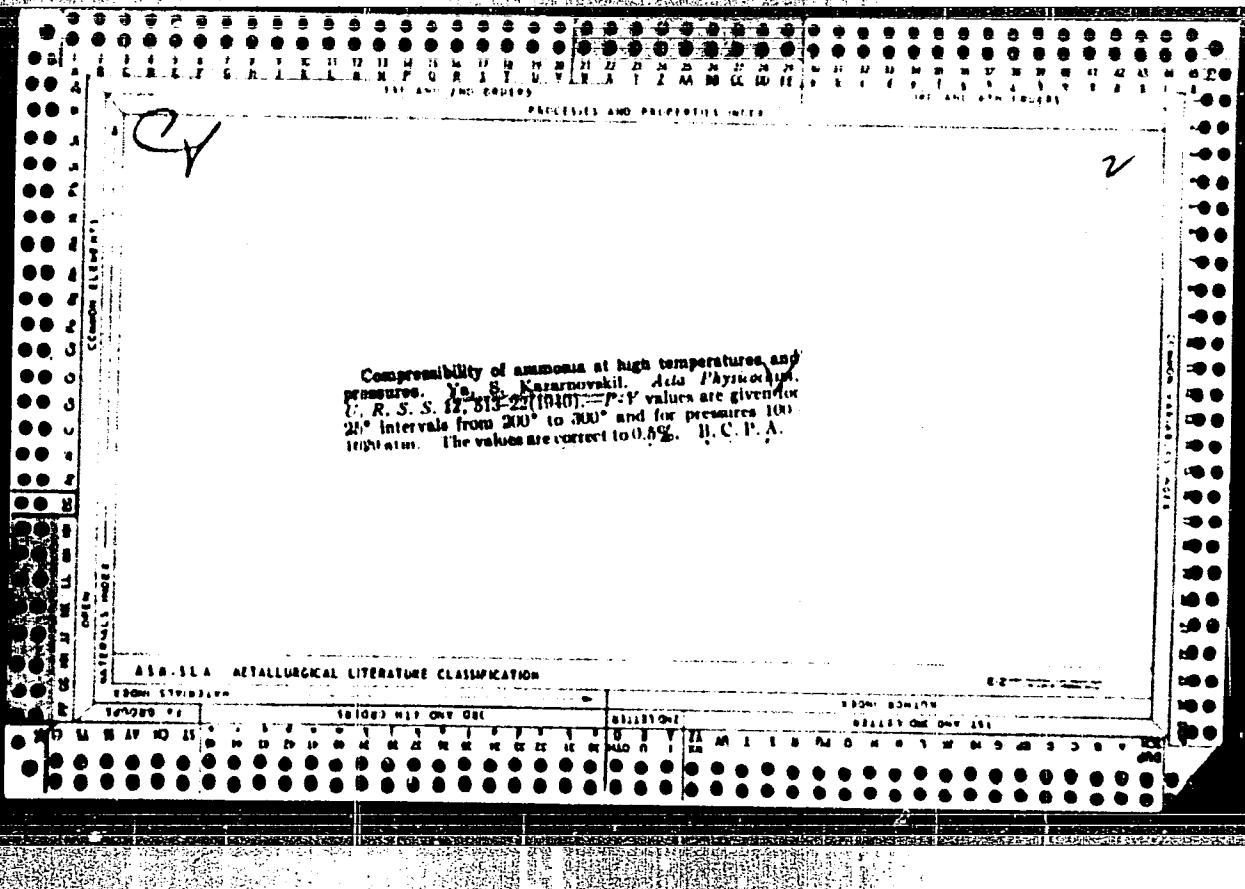
PAZARNOVSKIY Y.A.S.

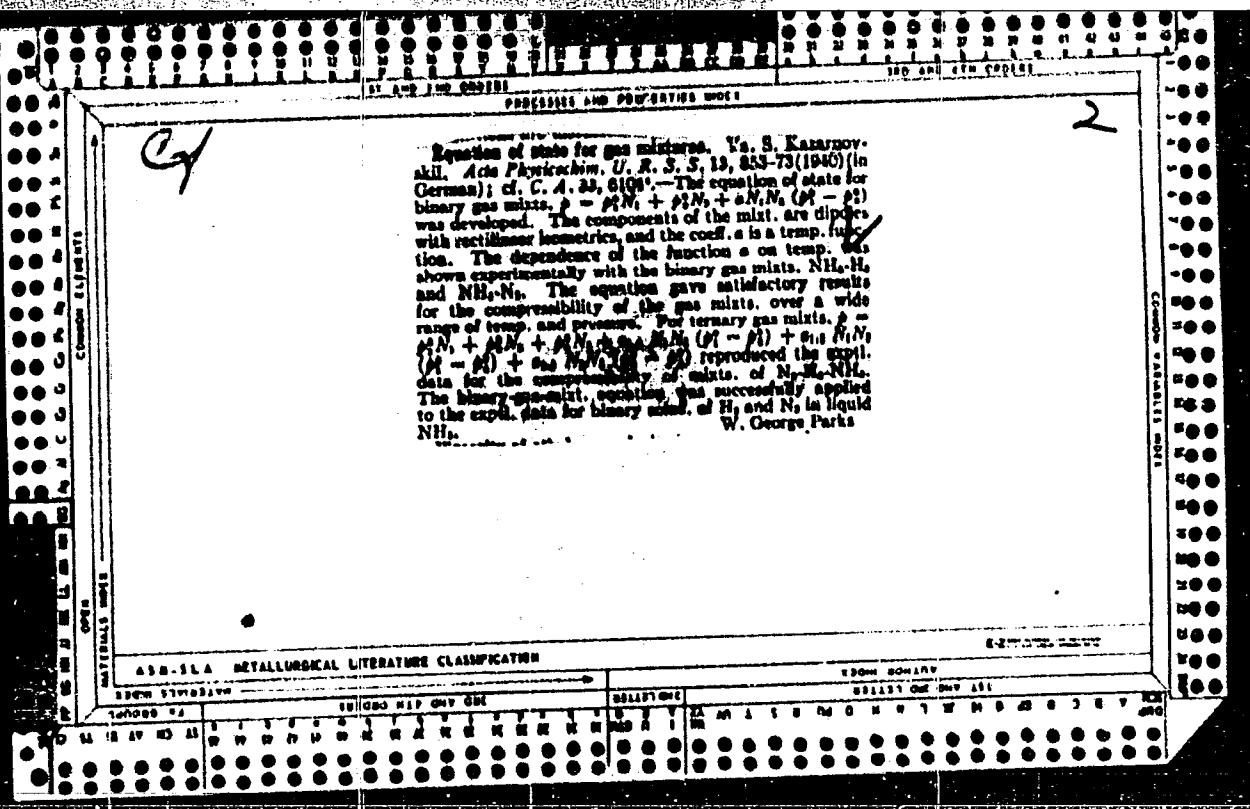
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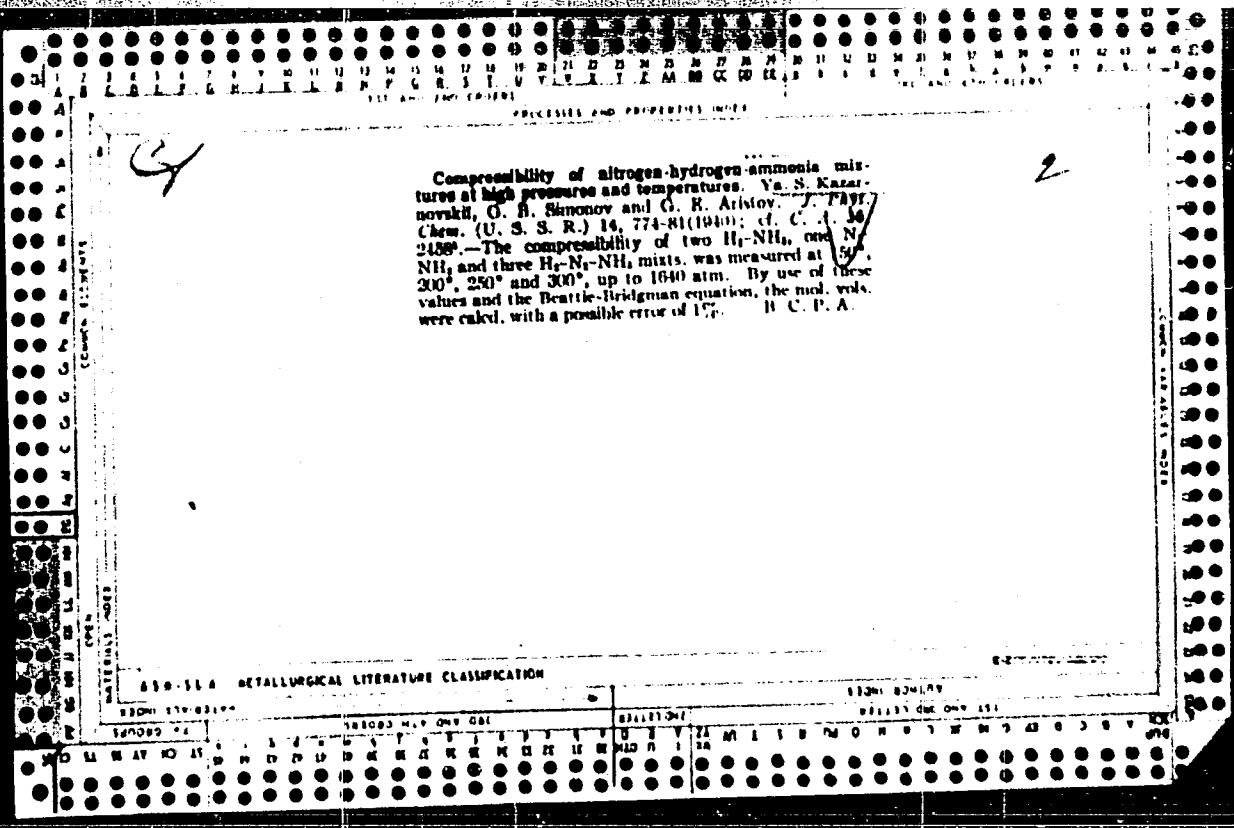
Equation of state for gas mixtures. I. R. KARABYUNIKI and J. N. KARABYUNIKI (J. Phys. Chem. Items., 1930, 13, 378-395).—A semi-empirical equation for the total pressure, p , of a binary gas mixture is proposed: $p = p_1^*N_1 + p_2^*N_2 + aN_1N_2(p_1^* - p_2^*)$, where p_1^* and p_2^* are the pressures of the components for a vol. equal to the mol. vol. of the mixture, N_1 and N_2 the mol. fractions of the components, and a is a const. which can be a function only of the temp. (cf. A., 1938, I, 611). It agrees with existing data for a wide range of temp., pressure, fugacity, and composition. R. C.

State Inst. of Nitrogen Industry, Moscow

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Equation of state for gas mixtures. J. S. Kharaschovskii (*J. Russ. Phys. Chem. Russ.*, 1900, 14, 1658-1667) - If all the pressures are given for the same mol. vol., the pressure of a mixture $p = p_1 N_1 + p_2 N_2 + \dots + p_n N_n$ (p_1, p_2, \dots, p_n , N_1, N_2, \dots, N_n being the pressures and mol. vol. of each component, and a a const.). In non-polar mixtures a is independent of temp.; in polar mixtures it depends on temp., but is independent of N^1 . The equation can also be applied to mixtures of a gas and a saturated vapour, e.g., to p of H_2 and NH_3 over liquid NH_3 . An analogous equation is valid for ternary mixtures. J. J. B.

J. J. B.

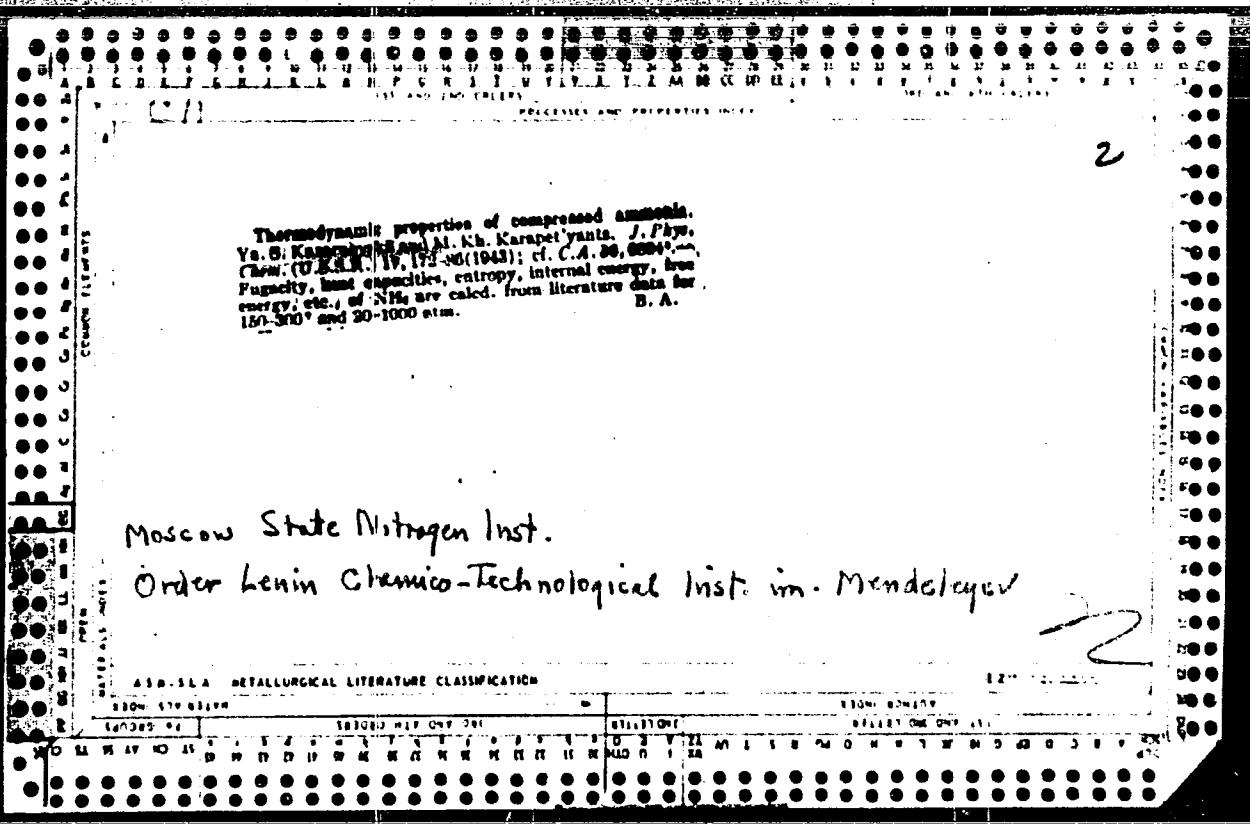
ASB 314 METALLURGICAL LITERATURE CLASSIFICATION

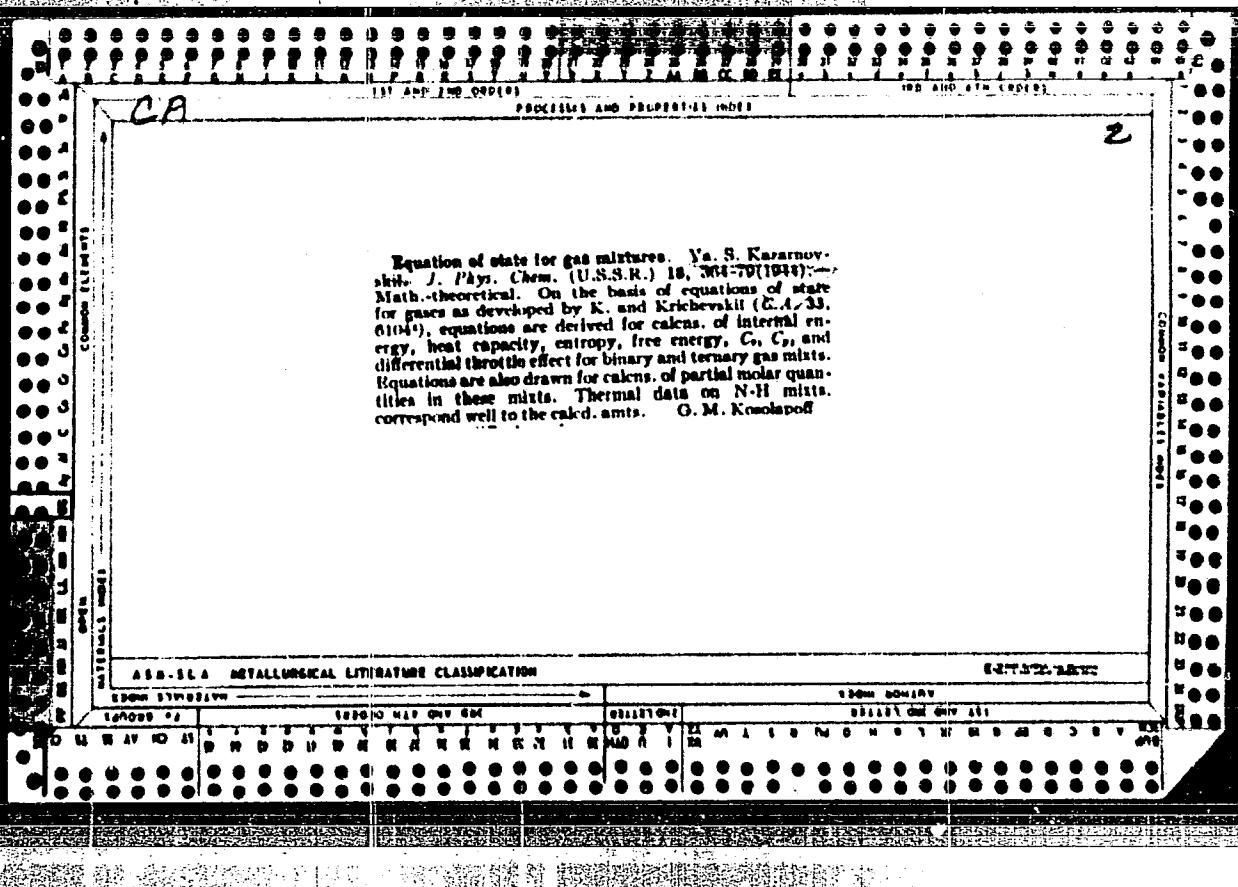
APPROVED FOR RELEASE: 06/13/2000

CIA-RDP86-00513R000721330005-0"

Effect of pressure on the heat of formation of ammonia.
Yu. S. Kazarinovskii and M. Kh. Khanapet'yan, *J. Phys. Chem. (U. S. S. R.)* 15, 600-73 (1941); cf. *C. A.* 35, 6190. The relation found by Gillespie and Brattie (*C. A.* 25, 342, 4172) using the Beattie-Bridgeman equation, for the heat of formation of NH₃ as a function of the pressure is incorrect. The equation for the heat capacity and compressibilities are not applicable. The calcs. of Kowalezyk (*C. A.* 28, 7135) are similarly incorrect because the values obtained for the compressibilities by use of the van der Waals equation differ from exptl. values by as much as 60 to 100%. The effect of pressure on the heat of the reaction $\frac{1}{2}N_2 + \frac{3}{2}H_2 = NH_3$ (all gases) at temps. from 250 to 600° and pressures up to 7000 atm. can, however, be calc'd. by means of the equation: $\Delta H_p = \Delta H_{p=1} + \int_1^p \Delta n \left(\frac{\partial \Delta H}{\partial p} \right)_T dp - T \int_1^p (\Delta \nu_r / \Delta T) dp$ and assuming that exptl. values for the compressibility of NH₃ up to 300° can be extrapolated to 500°. At high temps. and pressures the heat effect is about 20% greater than at atm. pressure. The heats of mixing of H N to form the three-component system H N NH₃ are calc'd. by use of the Krichevskii-Khasanova equation (cf. preceding abstr.).
P. H. Rathmann

APPENDIX A METALLURGICAL LITERATURE CLASSIFICATION





1345. COMPRESSIBILITY OF METHANE AND METHANE-AMMONIA MIXTURES AT HIGH TEMPERATURES AND PRESSURES. Kasarnovskii, I. S. and Levchenko, G. I. (J. Phys. Chem. (U.S.S.R.) 1944, 18, 380-2; U.O.P. Res. Lab. Abstr. 13 Feb. 1946, 21, 28) The compressibility of methane under pressures of 86.6 to 1400 atm. was determined at 250 and 300° C. The data at 200° C. agree well with those observed at low pressures by Kvalnes and Caddy, while some discrepancies were observed at 250 and 300° C. For determination of the compressibility of methane-ammonia mixtures the method of Michels was used. The binary mixtures contained respectively 32.84, 39.58, 53.85 and 55.72 per cent ammonia. The pressures used ranged from 82 to 1675 atm. and the temperatures from 150 to 300° C. The isometric graphs of the binary mixtures are straight lines within a wide interval of temperatures and pressures, which allows reliable extrapolation of these data to higher temperatures. The data obtained are quite satisfactorily represented by the equation of state for binary gaseous mixtures derived by Krichevskii and Kazarnovskii.

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KAZARNOVSKIYI, YA. S.

KRICHEVSKIYI, I. R., KAZARNOVSKIYI, YA. S., and
LEVCHENKO, G. T. (Nitrogen Inst. Moscow)
J. Phys. Chem. (USSR) 19, 314-22 (1945)
Thermodynamic properties of compressed nitrogen-
hydrogen mixtures.

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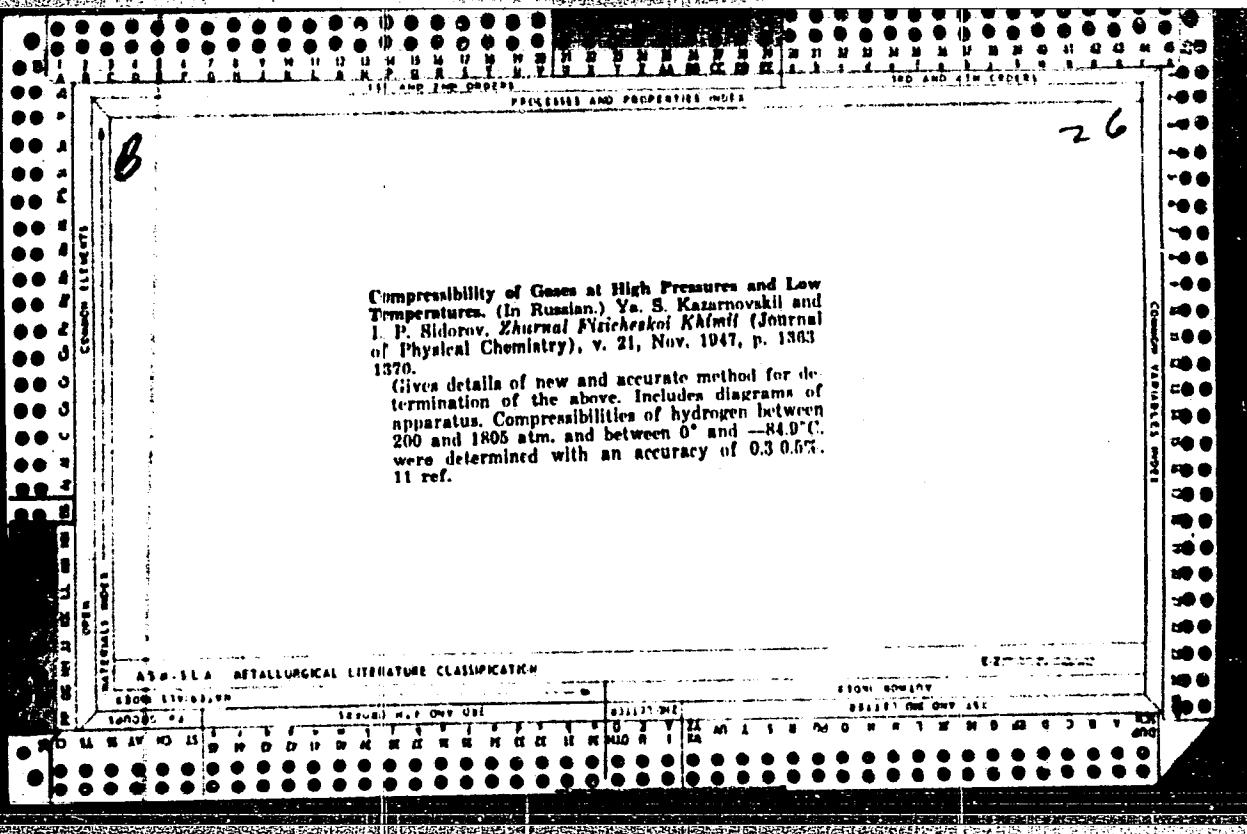
PROCESSES AND PROCESSES

Thermodynamic properties of nitrogen-hydrogen am monia mixtures. Va. N. Kazarinovskii (State Inst. Nitrogen Industry). *J. Phys. Chem.* (U.S.S.R.) 10, 382-404 (1945). For the mixt. NH_3 17.3%, N_2 20.0%, 19.18% the values of $d \log \rho / d \log T$, free energy, max. work, heat content, internal energy, and the two heat capacities are calcd. for the temp. range 150-300° between 80 and 1000 atm. From the heat-content data for the mixt. and its constituents the heat of mixing of NH_3 with $\text{N}_2 + 3 \text{ H}_2$ is calcd. If the heat of mixing is taken into account, the effect of pressure on the heat of NH_3 synthesis appears almost eliminated; the heat of reaction at 200° and 1000 atm. is only 8.4% higher than at the atm. pressure.

410-314 METALLURGICAL LITERATURE CLASSIFICATION

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KAZARNOVSKIY, Ya.S., kand.khim.nauk; SIDOROV, I.P., kand.tehn.nauk;
KAZARNOVSKAYA, D.B., kand.khim.nauk

Equilibrium of homogeneous gas reactions at high pressure.
Trudy GIAP no.7:21-25 '57. (MIRA 12:9)
(Phase rule and equilibrium) (Gases)

KOBOZEV, N.I., doktor khim.nauk; KAZARNOVSKIY, Ya.S., kand.khim.nauk;
MENDELEVICH, I.I., kand.tekhn.nauk

Explosive conversion of methane. Part 1. Trudy GIAP no.7:
155-166 '57.
(Methane) (Oxidation)

KAZARNOVSKIY, Ya.S., kand. khim. nauk; DEREVYANKO, I.G.; STEZHINSKIY, A.I.
DOROZHENOV, N.I., doktor khim. nauk

Explosive conversion of methane. Part 2. Trudy GIAP no.8:89-105
'57. (MIRA 12:9)
(Methane) (Gas and oil engines) (Fuel--Testing)

KAZARNOVSKIY, Ya.S., kand.khim.nauk; KOBZEV, N.I., doktor khim.nauk;
STRZHINSKIY, A.I.; TORBAN, B.S.

Explosive conversion of methane. Part 3. Trudy GIAP no.8:106-123
'57. (MIRA 12:9)
(Methane) (Gas and oil engines) (Fuel--Testing)

KAZARNOVSKIY, Ya.S.; KAREKHOV, N.V.

High-temperature conversion of gaseous hydrocarbons. Biul. tekhn.-
ekon. inform. no.8:12-14 '58. (MIRA 11:10)
(Hydrocarbone)

APPROVED FOR RELEASE: 06/13/2000 P.; CIA-RDP86-00513R000721330005-0"

KAZARNOVSKIY, Ya.S.; KAREKHOV, N.V.
SOLETSIEVA, I.N.

Oxidative thermal pyrolysis of hydrocarbon gases to acetylene.
Khim. prom. no. 7:547-551 O-N '60. (MIRA 13:12)
(Hydrocarbons) (Acetylene)

SEMELEV, V.P.; KAZARNOVSKIY, Ya.S.

High temperature conversion of individual hydrocarbons and
their mixtures. Gaz.prom. 5 no.3:33-40 Mr '60.
(MIRA 13:6)

(Gases--Analysis) (Hydrocarbons)

KAZARNOVSKIY, Ya.S.; SEMENOV, V.P.

High-temperature conversion of hydrocarbons. Gaz.prom.
5 no.7:41-50 '60. (MIRA 13:7)
(Hydrocarbons) (Oxidation)

S/064/61/000/001/002/011
B110/B215

AUTHORS: Kazarnovskiy, Ya. S., Semenov, V. P., Ovcharenko, B. G.,
Tsypin, A. N., Kolodeyev, I. P., Litvinchuk, V. A.

TITLE: Problems of apparatus design for the thermooxidative pyrolysis
of hydrocarbon gases

PERIODICAL: Khimicheskaya promyshlennost', no. 1, 1961, 11-15

TEXT: The pyrolysis of hydrocarbon gases for the production of C₂H₂ and synthesis gas takes place at 1450-1500°C. Since the intermediate C₂H₂ must not remain in the reaction zone for more than 0.003-0.01 sec, short tongues of flame must be used. As the traditional apparatus by Sachse and Bartholomé with maximum production of C₂H₂ of 3500-5000 tons per year is no longer sufficient, a new more efficient apparatus has to be designed. Highly turbulent combustion increases the rate of flame propagation and shortens the tongue considerably. The method of methane pyrolysis applied by B.S. Grinenko yielded high C₂H₂ concentrations. Its industrial application, however, is

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B110/B215

Problems of apparatus design for...

rendered difficult due to the almost critical velocity of the gas of 200-250 m/sec required for it, due to the high initial temperature ($700-800^{\circ}\text{C}$) of the oxygen necessary for the combustion stabilization (7% of the total amount), and due to an increase in temperature of the reaction channel of up to 2000°C . A pilot plant for average gas velocities and efficiencies of approximately $160 \text{ Nm}^3/\text{hr}$ is described. The conical ring nozzle of the burner contained whirl blades. The CH_4/O_2 mixture flowed into the reaction channel at 400°C and approximately 150 m/sec. The oxygen used for stabilization was only 5% of the total O_2 content. Maximum temperature in the reaction zone was 1450°C ; gas velocity: approximately 100 m/sec; its stay: 0.0025 sec. The acetylene yield was 8 to 8.4% of the reaction gases plus deposition of carbon black; 3 to 3.5 g/ Nm^3 of the initial mixture; ratio O_2 consumption = 0.62 to 0.64. According to the author, transition from pilot stage to industrial stage would be most suitable by increasing the number of burners. Fig. 1 shows the pilot plant of 1958. Coke oven gas of the ammonia unit compressed up to 0.36 atm by compressor (4), is purified in cloth filter (5).

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S/064/61/000/001/C02/011
B11C/B215

Problems of apparatus design for...

and conveyed to the preheating oven (3). Industrial oxygen compressed up to 0.38 atm by a XK -3 (ChK-3) compressor 1 is also conducted into the pre-heating oven via water separator (2) and filter (5). There, O_2 is heated to $350^{\circ}C$, and the coke oven gas to $450^{\circ}C$. From mixer (6), the mixture is at a temperature of $300^{\circ}C$ conducted into burner (7) and reaction vessel (8) from which the pyrolysis gases flow out at $80-90^{\circ}C$. After leaving scrubber (13) where the latter were purified from carbon black, they pass the water separator and filter before they are used for the production of acetylene. The triple burner of Fig. 3 which is used by the authors, has four spirals for producing whirls. Stabilizing O_2 is conducted through their axles. The following parameters have to be observed exactly to attain an optimum course of reaction: consumption of O_2 and hydrocarbon gas, temperature of pre-heating, ratios $[O_2] : [\Sigma C_1]^2$ in the initial mixture, and amounts of water. The following control and regulation apparatus were used: ДПМ -270 (DPM-270), ДП-410 (DP-410), ДП-280 (DP-280), М(Ш -ДР-54 (MSSh-Pr-54), ЭПП -09 (EPP-09), and 2 РЛ:24В (2RL:24V) on АУС (AUS) blocks. The following average composition

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S/064/61/000/001/002/011
B110/B215

Problems of apparatus design for...

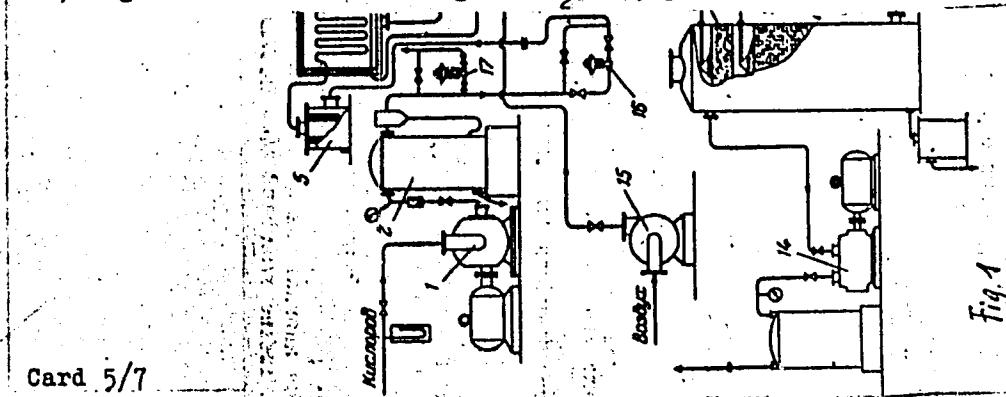
of the initial gas was determined: $C_2H_4 = 3\%$, $O_2 = 0.8\%$; $CO = 13.8\%$; $H_2 = 6.7\%$; $CH_4 = 62\%$; $N_2 = 13.7\%$. For stabilizing the flame, 3% of the total oxygen (79 to 98% of O_2) was required. The temperature of the reaction channel was approximately $1350^{\circ}C$, that of the reactor block $100^{\circ}C$. The total time of reaction was 5000 hr, ratios $[O_2] : [CH_4 + 2C_2H_4] = 0.62$ to 0.72. Optimum yield of $C_2H_2 = 7.3\%$, its average = 6.9%; total cracking = approximately 30%, effective cracking approximately 30%. The adiabatic temperatures of the reaction were lower than that of the hydrogen formation according to $CO + H_2O = CO_2 + H_2$. The temperature of preheating ($500^{\circ}C$) probably causes a reduction in O_2 consumption by 10%. The method is suited for supplementing the production of nitrogen fertilizers for which hydrogen is obtained from coke oven gases. A percentage of approximately 4 t of NH_3 per t of C_2H_2 was obtained. There are 3 figures, 2 tables, and 6 references: 4 Soviet-bloc and 2 non-Soviet-bloc.

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B110/B215

Problems of apparatus design for...

Legend to Fig. 1: basic diagram of a semi-industrial plant for the thermo-oxidative pyrolysis of hydrocarbon gases, 1) compressor XK-3 (KhK-3); 2) receiver-water separator, 3) oven for preheating gas 4) compressor PYTT (RUTT), 5) cloth filter, 6) mixer, 7) burner, 8) reaction vessel, 9) carbon black separator, 10) water seal, 11) bunker for carbon black (coke), 12) centrifugal pump, 13) scrubber, 14) gas pump FMK-4 (RMK-4), 15) air pump, 16) regulator for the ratio gas: O_2 , 17) pressure regulator.



Problems of apparatus design for...

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B110/B215

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Problems of apparatus design for...

S/064/61/000/001/002/011
B110/B215

Legend to Fig. 3: triple burner,
1) socket, 2) whirl spiral,
3) bottom of burner, 4) shell,
5) partition, 6) burner housing,
7) tube for stabilization oxygen,
a) water.

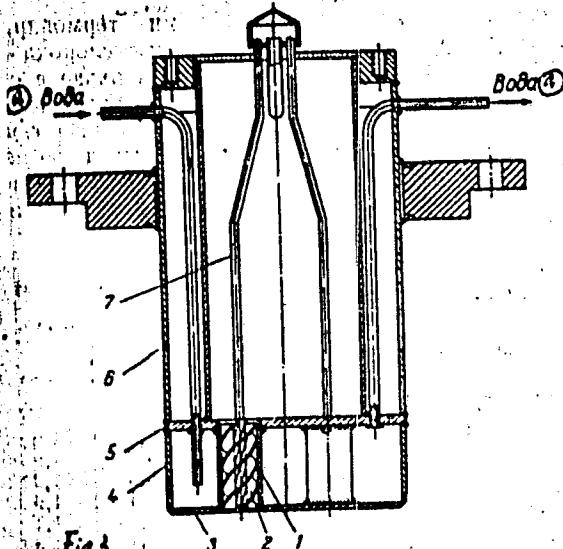


Fig.3

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SEMELEV, V.P.; KAZARNOVSKIY, Ya. S.; KOLODEYEV, I.P.; LITVINCHUK, V.A.

Processing of heavy petroleum residues into synthesis gas. Gaz.
prom. 6 no.2:41-48 '61. (MIRA 14:4)

(Gas manufacture and works)

S/081/61/000/020/083/089
B110/B147

AUTHORS: Semenov, V. P., Kazarnovskiy, Ya. S., Kolodeyev, I. P.,
Litvinchuk, V. A.

TITLE: Conversion of heavy petroleum residues into synthesis gas

PERIODICAL: Referativnyy zhurnal. Khimiya, no. 20, 1961, 405-406,
abstract 20M103 (Gaz. prom-st', no. 2, 1961, 41-48)

TEXT: Experiments on the conversion of mazout into synthesis gas were conducted on an experimental plant (diagram given) for conversion at high temperature. The efficiency of the plant was 6.6-7.9 kg of mazout per hr. The average ratio of the linear velocities of mazout escape from the nozzle and of the vapor-oxygen mixture was ~200, the volume of the reaction space was 0.006 m³, the temperature in the reaction zone was 1350-1450°C, and the linear velocity of converted gas in the reaction zone was 6-9 m/sec. Experimental and calculated equilibrium compositions of the reaction mixture, and comparative tables of efficiency with respect to carbon or oxygen, calculated from equations and obtained from the values of material equilibrium, are presented. It is concluded that

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Conversion of heavy petroleum...

S/081/61/000/020/083/089
B110/B147

the equations indicated for the techniques of commercial gas production from carbon raw material have a universal character. [Abstracter's note: Complete translation.]

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KAZARNOVSKIY, Ya.S.; OVCHARENKO, B.G.; SEMENOV, V.P.; DEREVYANHO, I.G.

Process gas obtained by the high temperature conversion of hydrocarbon gases. Gaz.prom. 7 no.1:43-50 '62. (MIRA 15:1)
(Gas, Natural) (Gas manufacture and works)

KAZARNOVSKIY, Ya.S.; KARKHOV, N.V.; KABANOV, F.I.; OVCHARENKO, B.G.

Production of synthesis gas by high temperature conversion of
hydrocarbon gases at high pressure. Khim.prom. no.6:396-404 Je
'62. (MIRA 15:11)

(Hydrocarbons) (Water gas)

KABANOV, F.I.; KARKHOV, N.V.; KAZARNOVSKIY, Ya.S.; OVCHARENKO, B.G.;
Prinimal uchastiye: ZUYEV, V.I.

Production of process gas by the high temperature conversion
of natural gas at elevated pressure. Khim.prom. no.9:547-555
Ag '62. (MIRA 15:9)

(Gas, Natural)
(Gas manufacture and works)

KAZARNOVSKII, Ya.S.; KAZARNOVSKAYA, D.B.; SIDOROV, I.P.

Equilibrium of homogeneous gas mixtures reactions at high
pressure. Khim.prom. no.10:747-750 O '62. (MIRA 15:12)
(Gases)
(Chemical equilibrium)

KAZARNOVSKAYA, D. B.; SIDOROV, I. P.; KAZARNOVSKIY, Ya. S.

Determination of the compressibility of methanol, carbon monoxide-hydrogen and carbon monoxide-hydrogen-methanol mixtures at high temperatures and pressures. Khim. prom. no. 3:205-211 Mr '63. (MIRA 16:4)

(Methanol) (Carbon monoxide) (Hydrogen)
(Compressibility)

KAZARNOVSKIY, Ya.S.; KAZARNOVSKAYA, D.B.; SIDOROV, I.P.

Equilibrium of the reaction of methanol synthesis from carbon monoxide and hydrogen at high pressure. Khim. prom. no.6:
426-433 Je '63. (MIRA 16:8)

(Methanol) (Carbon monoxide) (Hydrogen)

MIKHAYLOVA, S.A.; KAZARNOVSKIY, Ya.S.; KAZANOVSKAYA, D.B.

Thermodynamic properties of gaseous methanol at high
temperatures and pressures. Khim. prom. no.4:244-249
Ap '63. (MIRA 16:8)

KAZARNOVSKIY, Ya. S.; MIKHAYLOVA, S. A.; KAZARNOVSKAYA, D. B.

Influence of pressure on the thermal effect of the synthesis
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ACCESSION NR: AF5010546

UR/0064/65/000/004/0001/0006

AUTHOR: Aleynova, L. N.; Aleynov, D. P.; Kazarnovskiy, Ya. S.; Kornil'yev, P. M.

TITLE: Intermediate stages of partial combustion of methane with oxygen

SOURCE: Khimicheskaya promyshlennost', no. 4, 1965, 1-6

TOPIC TAGS: methane, combustion, kinetics, pyrolysis, combustion mechanism, partial combustion, acetylene

ABSTRACT: Partial methane combustion by thermooxidative pyrolysis is the basic process in the production of synthesis gas or acetylene from natural gas. The kinetics of partial methane oxidation at lower temperatures have been studied extensively by Semenov and coworkers. However, the mechanism proposed in these studies holds only at temperatures below 1000°C and cannot be applied to high temperature processes. Experiments were made with oxygen and natural gas in a flow reactor to determine the concentration of intermediates and reaction products (CO₂, acetylene, ethylene, ethane, propane, O₂, CO, H₂) as a function of methane conversion. Runs were made at initial gas temperatures of 25°C and 450°C and pressures of 1 and 4 atm. The general trend in the accumulation of intermediates was identical in both experiments. The results indicate that partial oxidation at high temperatures takes place in three stages: 1) methane oxidation, during which oxygen is

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used for conversion to CO, H₂, H₂O, and CO₂ while the acetylene accumulation remains low (0—0.65 conversion); 2) acetylene accumulation, during which the conversion is negligible, repair transient, 0.65—0.9 conversion; and 3) a final stage characterized by conversion to CO and H₂, cracking of acetylene, and a slight increase in conversion. The "NETRA" model is able to predict the behavior of the system under various conditions.

ASSOCIATION: none

SUBMITTED: 00

ENCL: 00

SUB CODE: PP

NO REF Sov: 015

OTHER: 014

ATT DPPRS 3231

Cord 2/2 f*

ALFEROV, L.R.; ALFEROV, D.L.; KAMARCHIKOV, V.A.; KURILYAN, R.Y.

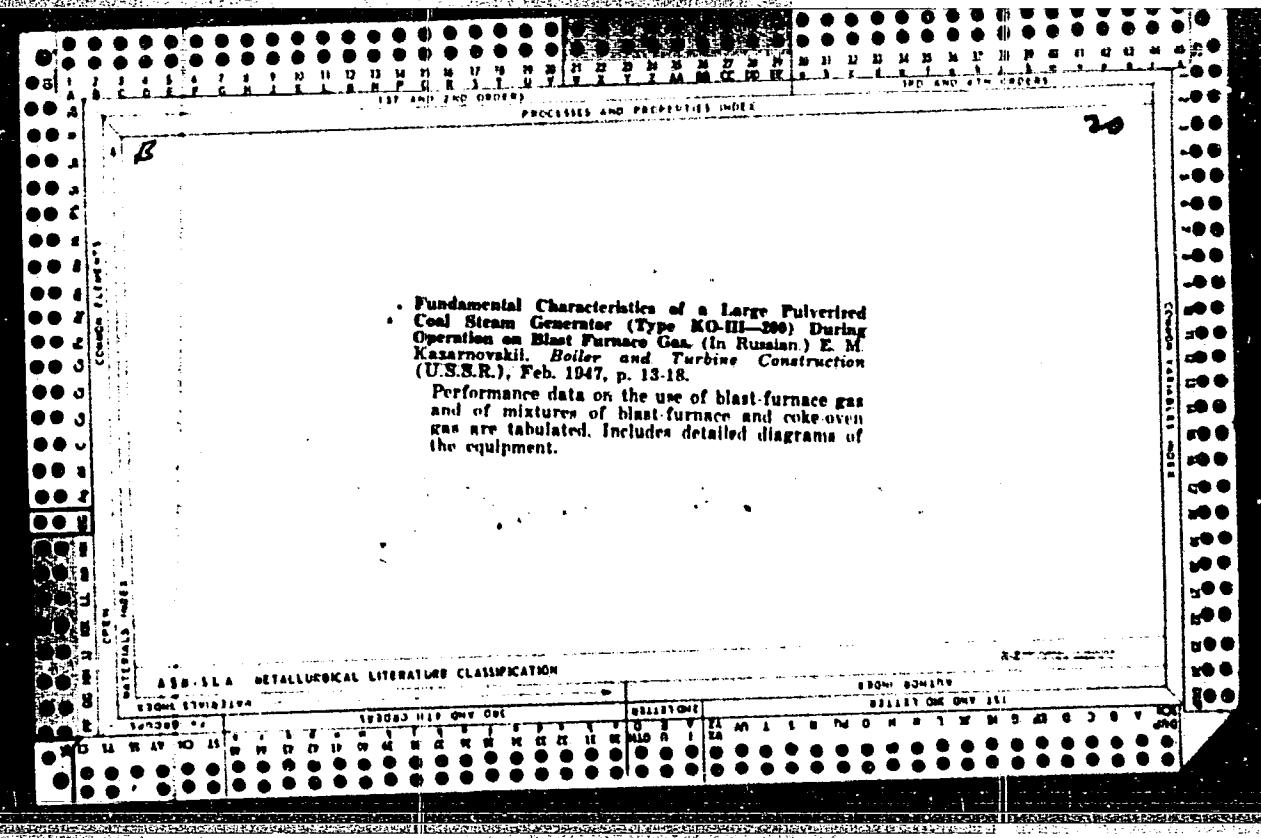
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USSR/Hydrology - Irrigation

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